

AMENDMENTS TO THE SPECIFICATION

Please delete the present Abstract of the Disclosure and replace it with the following new Abstract of the Disclosure.

A catalyst for deep desulfurization of a mineral oil corresponding to kerosene, ~~comprising~~having a nickel component of nickel and nickel oxide, zinc oxide, and aluminum oxide, ~~wherein the~~The content~~contents~~ of the nickel component, ~~in terms of nickel oxide is from 5 to 25% by weight and the content of the zinc oxide is from 30 to 70% by weight each based on the total of the content of the nickel component in terms of nickel oxide, the content of the zinc oxide, and the content of~~and the aluminum oxide and the zinc oxide are defined. ~~The the nitrogen monoxide adsorption of the catalyst at 1 kg/cm² (9.80×10⁻² MPa) and 40°C after hydrogen reduction at 360°C is 4.0 ml/g or more in terms of standard state, and the catalyst has a specific surface area of from 10 to 300 m²/g; are defined.~~ The the deep desulfurization catalyst, is which is obtained by carrying out an activation treatment, in the presence of hydrogen at a temperature of from 200 to 400°C and a pressure of from 1 to 20 kg/cm² (9.80×10⁻² to 1.96 MPa); a A process for producing the deep desulfurization catalyst is given and, comprising mixing a basic substance with each of an aqueous solution of a water soluble nickel metal salt and an aqueous solution of a water soluble zinc metal salt or with a mixed aqueous solution thereof to thereby form precipitates separately or simultaneously, and mixing the precipitates with aluminum oxide or an aluminum oxide precursor, followed by molding and burning; and a method of deep desulfurization is given,~~comprising bringing a mineral oil corresponding to kerosene into contact with hydrogen in the presence of the above deep desulfurization catalyst at~~

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~~a temperature of from 200 to 400°C, a pressure of from 1 to 20 kg/cm² (9.80×10^{-2} to 1.96 MPa),
and an LHSV (liquid hourly space velocity) of from 0.1 to 5.~~